

Modeling the dynamic mode of the chlorinator in the production of chloromethane

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In the production of chloromethane the main apparatus is a chlorinator, which in the production of chloromethane is used directly for chlorination of methane, this procedure requires a clear temperature regime, heating occurs by supplying heating gases from the furnace where the process of burning natural gas in excess air.

The main initial parameter (adjustable value) is the temperature of the reaction gases at the outlet of the chlorinator $\theta_{out_{p.r.}}$.

Inlet (control signal, control action) - air flow at the inlet to the furnace $G_{поб}$.
The perturbation is the consumption of reaction gases at the entrance to the apparatus $\theta_{in_{p.r.}}$.

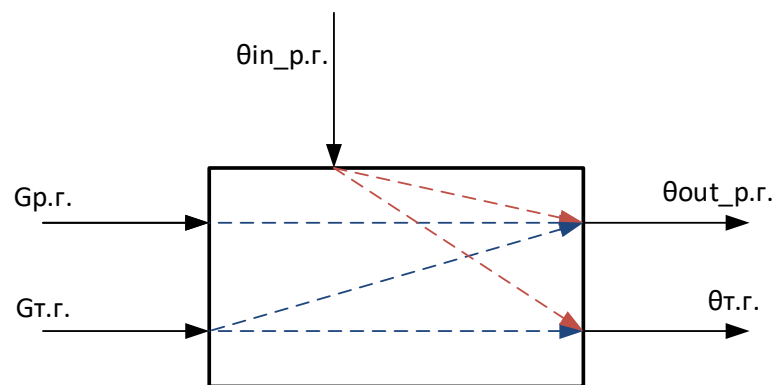


Fig. 1. Structural and parametric scheme of the chlorinator.

$G_{p.r.}$ – consumption of reaction gases; $\theta_{in_{p.r.}}$ – temperature of reaction gases at the inlet; $\theta_{out_{p.r.}}$ – temperature of reaction gases at the outlet; $G_{т.г.}$ – flue gas consumption; $\theta_{т.г.}$ – temperature of flue gases;

According to the technology of methane chlorination, it is necessary that the temperature of the reaction gases was 450 °C. Temperature control will be carried out through the channel «air flow - outlet temperature of reaction gases».

Equation of heat balances:

$$\begin{cases} G_{p.r.} \cdot c_{p.r.} \cdot \theta_{in_{p.r.}} + G_{т.г.} \cdot c_{т.г.} \cdot \theta_{т.г.} + q_r \cdot k \cdot x_b^m = G_{p.r.} \cdot c_{p.r.} \cdot \theta_{out_{p.r.}} \\ G_{п} \cdot c_{п} \cdot \theta_{п} + \alpha \cdot G_{поб} \cdot c_{поб} \cdot \theta_{поб} = G_{т.г.} \cdot c_{т.г.} \cdot \theta_{т.г.} \end{cases} \quad (1)$$

Table 1 Values of the main static mode

Name	Marking	Numeric value	Dimensionality
Consumption of reaction gases	$G_{p,r}$	0,5	kg / s
Flue gas consumption	$G_{T,r}$	0,02	kg / s
Fuel consumption	G_{Π}	0,02	kg / s
Density of flue gases	$\rho_{T,r}$	1,22	kg / m ³
Density of reaction gases	$\rho_{p,r}$	1,4	kg / m ³
Reaction gas temperature (inlet)	$\theta_{in,p,r}$	100	°C
Heat capacity of reaction gases	$c_{p,r}$	1.430	kJ / (kg · K)
Heat capacity of fuel	c_{Π}	2.226	kJ / (kg · K)
Heat capacity of air	$c_{\Pi OB}$	1.007	kJ / (kg · K)
Heat capacity of flue gases	$c_{T,r}$	20.07	kJ / (kg · K)
Energy of activation of a chemical reaction	E_a	83.7	kJ
Energy is attributed to 1 mole of substance	q_r	62.31	kJ
Volume of reaction gases	$V_{p,r}$	1.5	m ³
Volume of flue gases	$V_{T,r}$	2.5	m ³

From the equation of the second equation of the system (1) we derive the equation of dynamics, where the input parameter is $G_{\Pi OB}$, and the output – $\theta_{T,r}$:

$$G_{\Pi} \cdot c_{\Pi} \cdot \theta_{\Pi} + \alpha \cdot G_{\Pi OB} \cdot c_{\Pi OB} \cdot \theta_{\Pi OB} - G_{T,r} \cdot c_{T,r} \cdot \theta_{T,r} = V_{T,r} \cdot c_{T,r} \cdot \rho_{T,r} \frac{d\theta_{T,r}}{dt} \quad (2)$$

$$\Delta G_{\Pi} \cdot c_{\Pi} \cdot \theta_{\Pi} + \alpha \cdot \Delta G_{\Pi OB} \cdot c_{\Pi OB} \cdot \theta_{\Pi OB} - G_{T,r} \cdot c_{T,r} \cdot \Delta \theta_{T,r} = V_{T,r} \cdot c_{T,r} \cdot \rho_{T,r} \frac{d\Delta \theta_{T,r}}{dt} \quad (3)$$

$$\Delta G_{\Pi} \cdot \frac{c_{\Pi} \cdot \theta_{\Pi}}{G_{T,r} \cdot c_{T,r}} + \Delta G_{\Pi OB} \cdot \frac{\alpha \cdot c_{\Pi OB} \cdot \theta_{\Pi OB}}{G_{T,r} \cdot c_{T,r}} = \frac{V_{T,r} \cdot c_{T,r} \cdot \rho_{T,r}}{G_{T,r} \cdot c_{T,r}} \cdot \frac{d\Delta \theta_{T,r}}{dt} + \Delta \theta_{T,r} \quad (4)$$

$$T1 = \frac{V_{T,r} \cdot c_{T,r} \cdot \rho_{T,r}}{G_{T,r} \cdot c_{T,r}} \quad k_{Gt_\theta tg} = \frac{c_{\Pi} \cdot \theta_{\Pi}}{G_{T,r} \cdot c_{T,r}} \quad k_{Gair_ \theta tg} = \frac{\alpha \cdot c_{\Pi OB} \cdot \theta_{\Pi OB}}{G_{T,r} \cdot c_{T,r}} \quad (5)$$

Equations in canonical form

$$k_{Gt_t\theta g} \Delta G_{\Pi} + k_{Gair_t\theta g} \Delta G_{\Pi\Theta} = T1 \frac{d\Delta\theta_{\tau, \Gamma}}{dt} + \Delta\theta_{\tau, \Gamma} \quad (6)$$

Perform the transformation of equation (6) according to Laplace

$$\theta_{\tau, \Gamma} = \frac{k_{Gair_t\theta g} \Delta G_{\Pi\Theta}}{T1 \cdot p + 1} \quad (7)$$

Substituting in the first equation of the system (1) equation (7) we derive the equation of dynamics, where the input parameter is

$G_{\Pi\Theta}$, and the output – $\theta_{out_p, \Gamma}$:

$$G_{p, \Gamma} \cdot c_{p, \Gamma} \cdot \theta_{in_p, \Gamma} + G_{\tau, \Gamma} \cdot c_{\tau, \Gamma} \cdot \theta_{\tau, \Gamma} + q_r \cdot k \cdot x_b^m - G_{p, \Gamma} \cdot c_{p, \Gamma} \cdot \theta_{out_p, \Gamma} = V_{p, \Gamma} \cdot c_{p, \Gamma} \cdot \rho_{p, \Gamma} \frac{d\theta_{out_p, \Gamma}}{dt} \quad (8)$$

$$k = A \cdot e^{-\frac{E_a}{R \cdot \theta_{out_p, \Gamma}}} \quad (9)$$

$$y = G_{p, \Gamma} \cdot c_{p, \Gamma} \cdot q_r \cdot A \cdot E_a \frac{e^{\frac{E_a}{R \cdot \theta_{out_p, \Gamma}}}}{R \cdot \theta_{out_p, \Gamma}} \quad (10)$$

$$\frac{G_{p, \Gamma} \cdot c_{p, \Gamma}}{y} \cdot \Delta\theta_{in_p, \Gamma} + \frac{G_{\tau, \Gamma} \cdot c_{\tau, \Gamma}}{y} \cdot \Delta\theta_{\tau, \Gamma} = \frac{V_{p, \Gamma} \cdot c_{p, \Gamma} \cdot \rho_{p, \Gamma}}{y} \frac{d\Delta\theta_{out_p, \Gamma}}{dt} + \Delta\theta_{out_p, \Gamma} \quad (11)$$

$$k_{\theta_{in_G}} = \frac{G_{p, \Gamma} \cdot c_{p, \Gamma}}{y} \quad k_{\theta_{out_tg}} = \frac{G_{\tau, \Gamma} \cdot c_{\tau, \Gamma}}{y} \quad T2 = \frac{V_{p, \Gamma} \cdot c_{p, \Gamma} \cdot \rho_{p, \Gamma}}{y} \quad (12)$$

Equations in canonical form

$$k_{\theta_{in_G}} \cdot \Delta\theta_{in_p, \Gamma} + k_{\theta_{out_tg}} \cdot \Delta\theta_{\tau, \Gamma} = T2 \frac{d\Delta\theta_{out_p, \Gamma}}{dt} + \Delta\theta_{out_p, \Gamma} \quad (13)$$

Perform the transformation of equation (13) according to Laplace

$$(T2 \cdot p + 1) \Delta\theta_{out_p, \Gamma} = \frac{k_{\theta_{out_tg}} \cdot k_{Gair_t\theta g}}{(T1 \cdot p + 1)} \Delta G_{\Pi\Theta} \quad (14)$$

$$\frac{\theta_{out_p, \Gamma}(p)}{\Delta G_{\Pi\Theta}(p)} = \frac{k_{\theta_{out_tg}} \cdot k_{Gair_t\theta g}}{(T1 \cdot p + 1)(T2 \cdot p + 1)} \quad (15)$$

According to the results of the transformations, the transfer function of the system via the control channel «air flow - the temperature of the reaction gases at the outlet» was obtained.

$$W(p) = \frac{k_{\theta_{out_tg}} \cdot k_{Gair_t\theta g}}{(T1 \cdot p + 1)(T2 \cdot p + 1)} \quad (16)$$

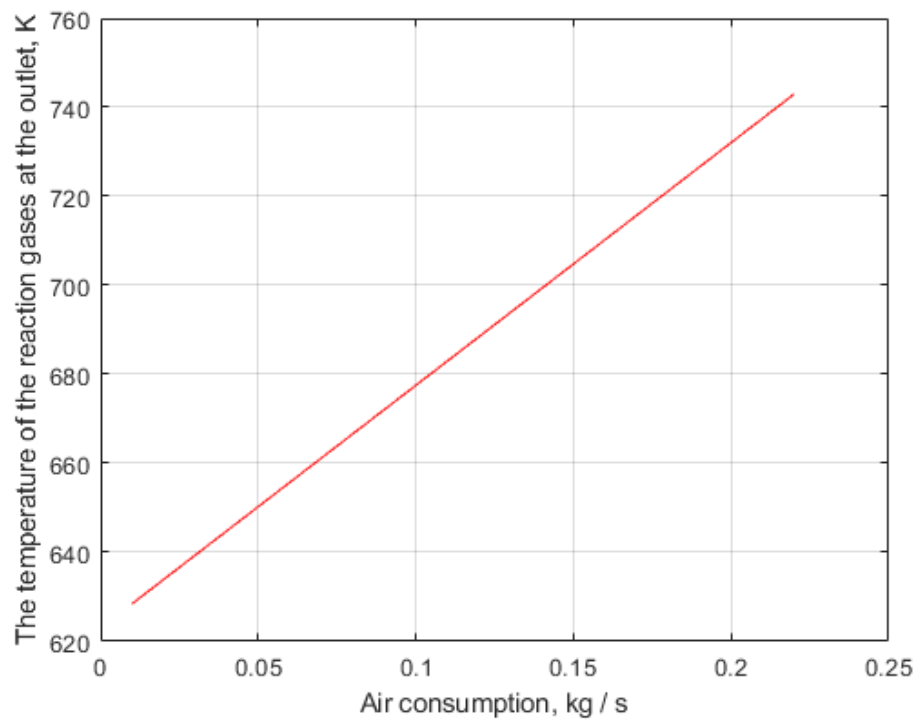


Fig. 2 Static characteristic on the channel $G_{\text{пов}} \rightarrow \theta_{\text{out}_{\text{п.г}}}$

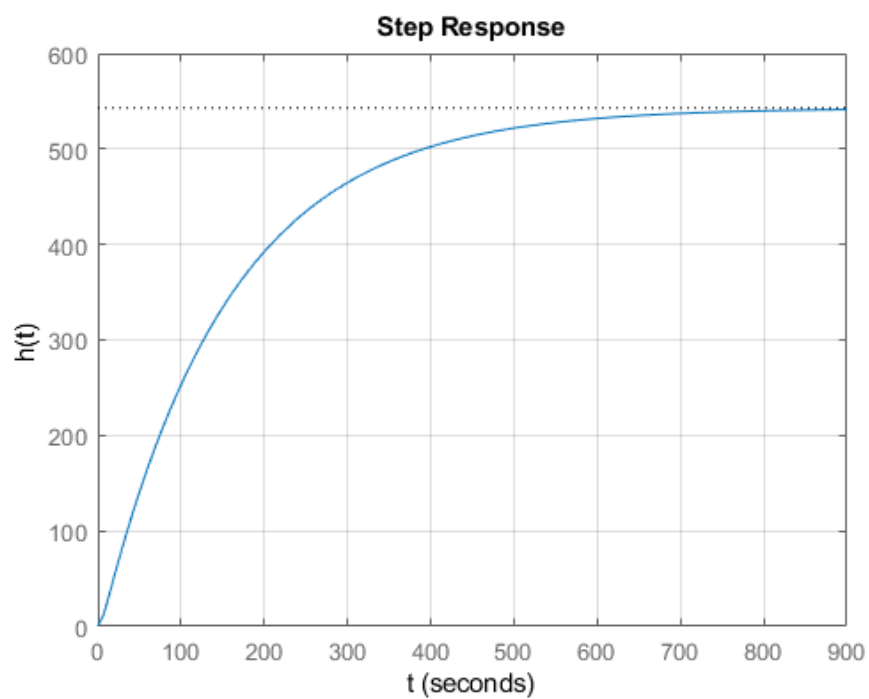


Fig. 3 Dynamic characteristic on the channel $G_{\text{пов}} \rightarrow \theta_{\text{out}_{\text{п.г}}}$

Literature

1. Юкельсон И. И. Технология основного органического синтеза. Москва: Химия, 1968.848с.